Original Research

Study of Bioretention System on Heavy-Metal Removal Effect

Zengchao Liu^{1,2}, Jiake Li^{1*}, Peng Li¹, Yajiao Li³, Wenying Li¹

¹State Key Laboratory Base of Eco-Hydraulic Engineering in Arid Area, Xi'an University of Technology, Xi'an 710048, China

²School of Materials Science and Chemical Engineering, Xi'an Technological University, Xi'an 710021, China

³School of Architecture and Civil Engineering, Xi'an University of Science and Technology, Xi'an 710054, China

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Abstract

Bioretention is a typical low-impact development (LID) technology. This work used four different filler combinations of bioretention tank pilot test devices. Experiments on influence factors and intermittent operation were conducted. A continuous-run experiment was also performed to determine the purification ability of bioretention system on heavy metals. Results showed that the removal efficiency of heavy metals by fly ash tank was the most efficient, with a removal rate reaching 85.57%. The removal effect on high-influent concentrations in filter was better than that in low-influent concentrations. With increased rainfall time intervals (antecedent dry time), heavy-metal removal efficiency improved. Temperature did not affect the removal efficiency of heavy metals on the whole based on the long duration of intermittent operation experiments. Moreover, the effluent heavy-metal concentration presented a descending trend during each simulation rainfall runoff event. During continuous operation test, heavy metals did not reach the exhaustion point in the experimental tanks, while the effluent concentration increased with increased water volume. According to PLS regression analysis, rainfall time interval was the most important factor affecting Zn removal rate, followed by filler characteristics, influent volume, and influent concentration.

Keywords: bioretention, low-impact development, influence factor, removal efficiency

Introduction

Urban growth and development negatively affect nearby natural water systems. For example, increases in impervious land areas decrease rainfall infiltration, increase runoff rates and volumes, and decrease runoff travel time. In addition, detrimental water quality changes in stormwater runoff accompany land-use changes that coincide with urbanization [1].

In addition, due to human activities, atmospheric deposition, and other factors, a large number of pollutants accumulate and are discharged into the municipal stormwater sewer by stormwater runoff flushing, then enter the receiving waterbody [2]. Although low concentrations of some heavy metals such as copper (Cu) and zinc (Zn) are essential to plants, humans, and animals, high heavy metal concentrations are toxic [3]. Lead (Pb), on the other

^{*}e-mail: xaut ljk@163.com

hand, can have negative effects even at low concentrations [4]. Therefore, heavy metal concentrations in stormwater runoff raise a serious threat, especially for aquatic organisms [5]. Consequently, it is vital to control and reduce heavy metal concentrations in urban stormwater runoff. In order to develop an effective removal strategy of heavy metals in water resources, a number of aspects must be evaluated [6].

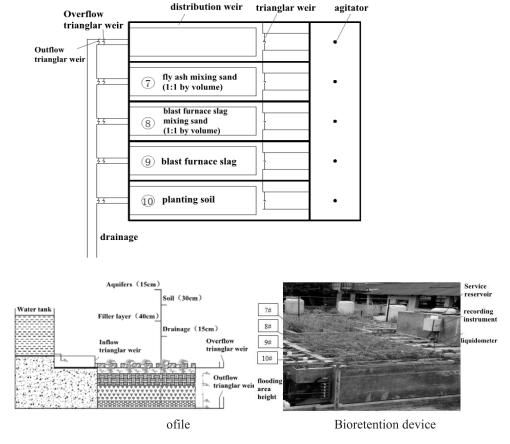
Bioretention basins, also called rain gardens, have become a frequent best management practice (BMP) to retain pollutants from road runoff. Stormwater enters a bioretention unit and is purified by physical filtration, adsorption, and ion exchange of soil, microbial transformation and redistribution, evaporation and absorption of plants in the soil and filler layers [7-8]. Laboratory and pilot-scale bioretention box studies have shown that removal efficiencies of Zn, Cu, and Pb from a synthetic runoff were typically greater than 95%. The removal rate of total phosphorus and total Kjeldahl nitrogen was approximately 80% and 50-70%, respectively [9]. Different types of purification effect of heavy metals by bioretention medium, and heavy metals in bioretention medium inside the geometrical shape, accumulation, migration characteristics, and lack of related research, the combination packing is different, and a different blending ratio will affect the removal efficiency of heavy metals by the bioretention system. In this paper, the removal effect of the bioretention retention system on heavy metal, the factors affecting the removal efficiency, and the comparison of intermittent operation and continuous operation are studied to promote better development of bioretention systems.

Materials and Methods

Device Setup

Ten bioretention tanks from Nos. 1 to 10 were designed and constructed at an outdoor testing ground of the Key Lab of Northwest Water Resource and Environment Ecology of the Ministry of Education at Xi'an University of Technology in 2013, and each tank had a different structural configuration. Of them, the filler structures of bioretention tanks 7-10 are typical and representative and were therefore selected for the experiments. Bioretention tanks 7, 9, and 10 were used for the experiments of influence factors. Meanwhile, bioretention tanks 7 and 10 were used for the continuous operation experiment. Bioretention tank 8 was used for the intermittent running experiment across different seasons. Experimental bioretention tanks are rectangular in shape (2 m long, 0.5 m wide, and 1.05 m deep; Fig. 1a). Ligustrum quihoui and Ophiopogon japonicas are planted in the tanks, which

Vertical



Inflow

Water

Fig. 1. Bioretention test equipment.

P(a)q (L/s.ha) F(ha)V(L)t (min) Level φ 52.0922 5 120 0.9 0.0017 573.8472 High 2 0.9 0.0017 427.1591 120 38.7762 Middle 0.5 0.9 0.0017 120 18.6300 205.2285 Low

Table 1. Experimental simulated influent water volumes.

Note: P-Return period, t-Duration of rainfall, q-Rainfall intensity, ϕ -Runoff coefficient, F- Catchment area, V-Influent volume of bioretention tank

are common greening plants. A 30° triangular weir was installed on the inlet, outlet, and overflow outlet in the bioretention tank (Fig. 1a). There is an XTHJ-recorder before every weir to monitor the flow of water in the inlet, outlet, and overflow. The structural configuration was aguifer layer (15 cm), planting soil (30 cm), artificial fillers (40 cm), and gravel drainage layer (15 cm) from top to bottom. Artificial fillers in tanks 7-10 consisted of fly ash mixing sand (1:1 by volume), blast furnace slag mixing sand (1:1 by volume), blast furnace slag, and planting soil, respectively. The bottom of the gravel drainage is layered perforated pipes, and the drain was cupped by permeable geotextile. Between each layer of packing are permeable geotextile and various tanks; besides, the artificial packing layer is not the same as the others and its thickness in each layer is consistent (see photo in Fig. 1c).

Monitoring and Analysis Methodology

The experiment took copper (Cu), zinc (Zn), and cadmium (Cd) as the main analysis targets. The assumed rainfall intensities of the experiment were calculated through the rainstorm intensity formula of Xi'an city under three return periods of 0.5a, 2a, and 5a [10]. Then the rainfall was obtained with rainfall duration of 2 h. The influent water volumes of the tanks were calculated through the rainfall multiplying catchment area. The results are shown in Table 1. In this research, influent concentrations remained constant. The concentrations of water distribution were referred to the earlier period monitored results by our research group on urban rainfall runoff pollution [11] (Table 2). This experiment released the water according to the rainfall pattern in Chicago [12], with the rainfall peak coefficient at 0.3, simulating a complete rainfall process. This Chicago process could meet the general requirements for accuracy, which is widely used at home and abroad.

The $0.45~\mu m$ filter was used to filtrate the sample; heavy metal concentration was then determined via an AAS Zeenit 700 atom absorption spectroscope. Quantitative analysis for the purification effect of the bioretention system was carried out via Equations 1 and 2.

$$R_{\rm i} = \frac{C_{\rm in} - C_{\rm out}}{C_{\rm in}} \times 100\% \tag{1}$$

$$R_{\rm c} = \frac{1}{m} \sum_{i=1}^{m} R_i \tag{2}$$

...where R_i = each of the characteristics of pollutants' (Cu, Zn, and Cd) removal rates, R_c = the average removal rate of each pollutant, and m = total number of samples collected during the event.

Experimental Scheme

Experiments of Influence Factors

Bioretention tanks 7, 9, and 10 were moistened using tapwater before each test. Nine tests were conducted to investigate the tank operation effect with different filler combinations, influent concentrations, and rainfall time intervals (antecedent dry time). Through these experiments, the characteristics and laws of bioretention cells on heavy metal pollutant removal were summarized. The specific experimental arrangement is shown in Table 3.

Intermittent Operation Experiments

The bioretention tank operation effect changes and tendencies were studied under the conditions of Xi'an

Table 2. Experimental simulated influent concentrations.

Pollutants	COD	NO ₃ -N	NH ₃ -N	TP	Cu	Zn	Cd
High concentration (mg/L)	600	14	6	2.5	0.1	1.5	0.05
Medium concentration (mg/L)	300	8	3	1.0	0.05	0.8	0.03
Reagent	$C_{6}H_{12}O_{6}$	KNO ₃	NH ₄ Cl	KH ₂ PO ₄	CuCl ₂	ZnSO ₄	CdCl ₂

Table 3. Design of influence factor experiments.

Number of water quality test	Concentration of pollutants	The height of submerged zone /(mm)	Intervals /(d)	Experimental date	Water quantity /(L)
clean water experiment	-	-	-	-	-
Test 1	medium	0		2015-5-20	573.8472
			7		
Test 2	medium	150		2015-5-27	573.8472
			7		
Test 3	medium	0		2015-6-03	573.8472
			15		
Test 4	medium	0		2015-6-18	573.8472
			7		
Test 5	medium	0		2015-6-25	573.8472
			3		
Test 6	medium	0		2015-6-28	573.8472
			7		
Test 7	medium	0		2015-7-05	427.1591
			7		
Test 8	medium	0		2015-7-12	573.8472
			7		
Test 9	high	0		2015-7-19	573.8472

climate (plant transpiration, evapotranspiration, and soil restores). Bioretention tank 8 was selected to perform the intermittent operational experiment with medium influent concentration at the 5a return period rainfall. Intermittent operation started from May 2015 to December 2015, and the simulated rainwater experiment was conducted on tank 8 (artificial filler layer is a mixture of blast furnace slag and sand with the ratio 1:1) every 30 days and lasted for eight months. There were eight water quality tests.

Continuous Operational Experiments

During the period of rainfall, filters mainly depend on adsorption and precipitation via the padding to remove the runoff pollutant. To study the exhaustion performance of filler, a penetration curve graph was used. That is, under continuous inflow, the padding adsorption exhaustion point was determined through comparing the influent concentration and effluent concentration. Tanks 7 and 10 were selected to do the experiments, and influent concentration was kept at medium. Considering that continuous dewatering may make padding lose its adsorption capacity after several hours, the influent load transitioned gradually from small to heavy. Two tanks were all running for 24 h with a 0.5-year return period influent volume, 12h with a two-year return period influent volume, and 8 h with a five-year return period influent volume. The influent concentration was constant, and

the valve opening also remained constant. The influent samples were taken every 2 h, and the effluent samples were taken every 0.5 h when the water started to flow out; water sample concentrations in different times were then determined. If the $C/[C_0(1-10\%)] \ge 1$ for three consecutive hours, the capacity of packing was depleted.

Results and Discussion

Influence Factor Result Analysis

The primary factors influencing the removal effects of bioretention tank on heavy metal include padding combination, pollutant concentration, rainfall time interval, and so on. Tanks 7, 9, and 10 were selected to determine the important order of these influencing factors. The evaluation index is the pollutant concentration removal rate.

Filler Combinations

The simulation dry time of tests 3, 5, and 8 before the rainfall is 7 d; the influent concentration is medium concentration and five-year return period of rainwater. The test results are shown in Fig. 2.

Fig. 2 shows that the removal effect of Cu is better than those of other heavy metals, and partial effluent

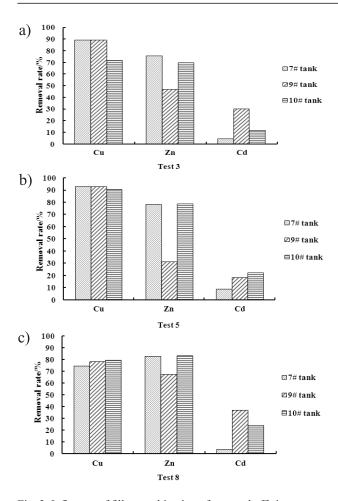


Fig. 2. Influence of filler combination of removal efficiency.

concentrations were lower than the detection limit of an atomic absorption spectrophotometer (AAS Zeenit700). The removal effects of Cu in three tanks (7, 9, and 10) were similar. Of them, tank 7 (packed with fly ash mixing sand) is the most efficient, with an average elimination rate of 85.57%. The removal effect of Zn in tanks 7 and 10 (packing with planting soil) were similar, with the average elimination rates of 78.83% and 77.17%, respectively. Zn removal effect in tank 9 (packed with blast furnace slag) is relatively poor, with an average removal rate of 48.4%. Heavy metals were always purified through the interception of surface materials, internal physical adsorption, and absorption of plants in bioretention, and most of the particulate heavy metals in rainwater were adsorbed on suspended solids, then removed through filtration [13]. In urban rainwater runoff, Cu, Zn, Pb, and Cd particulates respectively account for 67%, 52%, 97%, and 83% of the total [14]. However, the dissolved Zn contributes most of the total. A number of studies have indicated that the metal competitive sorption would be in the order of Pb>Cu>Zn [15]. But elimination effects of Cd in these three tanks were not very efficient, which may be due to too low influent Cd concentration and close to the detection limit of atomic absorption spectrophotometer. Compared with other tanks, tank 9 (packed with blastfurnace slag) was good at the removal of Cd. Overall, the

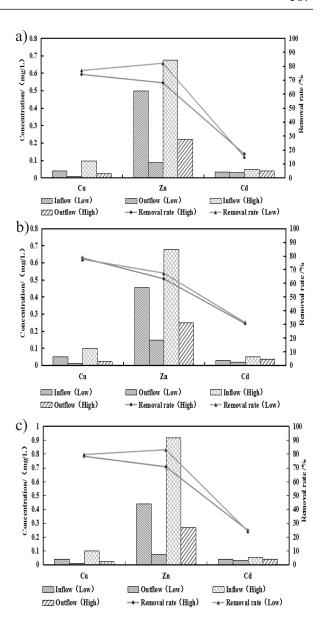


Fig. 3. Effects of removal efficiency on heavy metals with different bioretention media: a) Tank 7, b) Tank 9, c) Tank 10.

removal rates of heavy metal at bioretention tanks 7 and 10 were great.

The Rainfall Runoff Concentration of Heavy Metals

With two inflow concentrations of medium and high (Table 3), the removal effects of different media on two heavy metals concentrations were obtained from tests 8 and 9, which were shown in Fig. 3.

The effluent concentration of each heavy metal increased with the increase of influent concentration, while the removal rates of Cu and Cd at high influent concentration did not differ significantly with those at low influent concentration. For tanks 7, 9, and 10, the removal rate of Cu was above 75%, and that of Cd was about 20%.

Although the removal rate of Zn was affected by influent concentration in tanks 7 and 10, it was not affected by influent concentration in tank 9. The removal rate of Zn under low influent concentration was higher than that under high influent concentration, and the minimum removal rate of Zn was 63%. On the whole, the influent concentration of heavy metals had little effect on the removal efficiency of the bioretention system.

Rainfall Time Interval

Tests 4-6 were used to study the influence of rainfall time interval on the removal effect. The experimental conditions of the three tests are: medium influent concentration, five-year return period inflow water volume, and rainfall time intervals of 15 d, 7 d, and 3 d. The experimental results are shown in Fig 4.

The changes of removal rate with rainfall time interval for Cu, Zn, and Cd in tanks 7, 9, and 10 are shown in Fig. 4. The removal rate changes of Cu and Zn are obvious

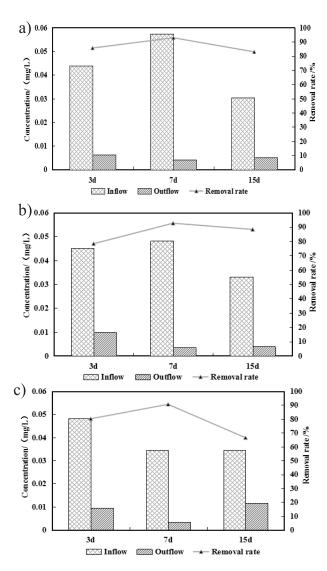


Fig. 4. Effects of rainfall interval on heavy metals with different bioretention media: a) Tank 7, b) Tank 9, c) Tank 10.

with test time interval in the three tanks. With the increase of rainfall time interval, the removal rate of Cu in the three tanks first increased and then decreased. The removal efficiency of Cu was best when the interval of rainfall was seven days and the average removal rate was above 90%. The removal rate of Zn in the three tanks increased with the increase of rainfall interval. The highest removal rate was observed when the rainfall interval was 15 days, and the highest removal rate of tank 7 was 87%. The Cd removal rates in the three tanks had no obvious changes with time interval, and the time interval had little influence on the removal of Cd. In general, the rainfall time interval has a great impact on heavy-metal removal efficiency. The longer the time interval, the higher the heavy metal removal rate. Dryness may affect soil structure (e.g., porosity increase and cracking occurrence) and plant activity, including removal efficiency of heavy metals [16]. Although the literature [17] showed that short-term dryness had no effect on heavy metal removal, effluent heavy metal concentration increases after three weeks; in the case of a submerged area and carbon source, however, even if the dry period had been extended, Cu and Pb still maintained the best removal rates.

Testing the Effect of Intermittent Operation

We conducted eight water quality tests. The experimental conditions were medium inflow concentration, and 2 h rainfall runoff inflow water volume with five-year return period. For each test, inflow water volume, influent heavy metal concentration, and the antecedent dry time were kept consistent. The influences of weather conditions and padding properties on the purification effect of tanks were compared.

Concentration Removal Rate

Fig. 5 shows the pollutant removal effect having no certain tendency. The entire experiment underwent high and low temperature seasons. The eight-month-long water quality purification effects demonstrated that the removal rates were 70.3-86% for Cu, 37.5-79.4% for Zn, and 20.2-39.5% for Cd. Accordingly, temperature had little influence on the retention tank purifying heavy metal.

Concentration Process Line

For different heavy metals, a bioretention system has different removal effects, and effluent concentrations present different rules. The concentration process line is shown in Figure 6. The influent concentration during each test was constant. Effluent samples were collected once every 15 minutes after outflow was discharged, then the sample concentrations were examined.

Heavy metals of urban stormwater runoff are removed by intercepting surface media, physisorption of internal media, and absorption of plants in the bioretention system [18]. Laboratory studies on heavy metal removal rates

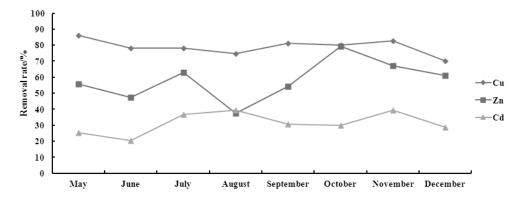


Fig. 5. Removal effects of pollutant concentrations.

in stormwater show that most of the heavy metals were removed on the surface of media; even the removal rate of the filter layer without plants is higher than that with plants [6]. Therefore, the removal of heavy metals of stormwater runoff by bioretention media had definite selectivity. In addition, plants and their roots have important effects on dissolution and migration of heavy metals in the soil. As shown in Fig. 6, in the eight water quality tests using tank 8, the effluent concentrations of Cu and Zn showed

a decreasing trend. Due to low influent Cd concentration, effluent Cd concentration was unstable. However, it was decreased on the whole. In general, the bioretention tank has good removal efficiency for heavy metals.

Continuous Operation Test

The artificial packing layer of tank 7 is fly ash with sand, and it has good water quality purification effect in

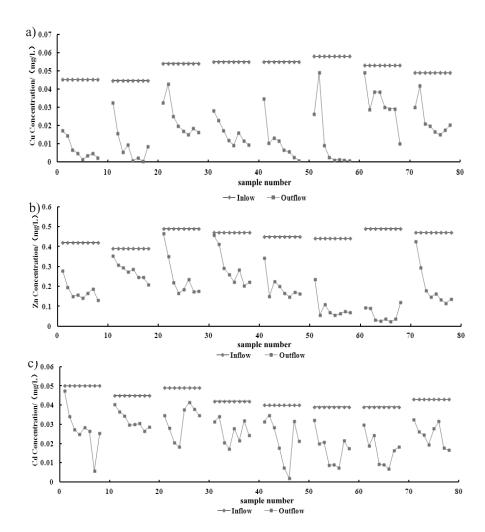


Fig. 6. Concentration process line of outflow pollutants.

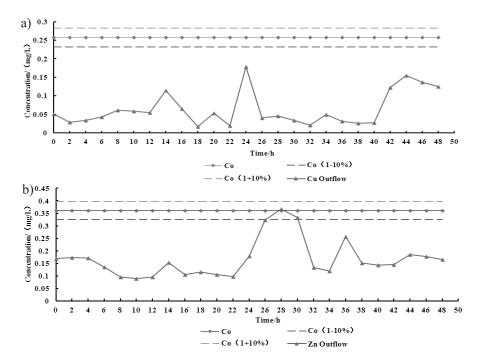


Fig. 7. Exhausted experiment result of No. 7 bioretention tank

the previous tests mentioned above. Therefore, tank 7 was selected to conduct a continuous operation test to observe the purification ability of bioretention, and the results are shown in Fig. 7.

In Fig. 7a), Cu did not reach the exhaustion point of media in tank 7 during the whole test process. The effluent concentration of Cu increased with increasing influent volume, which may be due to Cu absorbed on the surface of the filler particles or soil being washed down by strong water flow. In Fig. 7b), under small

hydraulic load, effluent concentrations of Zn are stable and low. The phenomenon of $C>[C_0(1-10\%)]$ for Zn appeared after 26 h. Under medium hydraulic load, the effluent concentrations of Zn are relatively high. While under large hydraulic load, Zn returns to a low effluent concentration.

The artificial packing layer for tank 10 is planting soil, which has good removal for heavy metal, as shown in Fig. 8. Under low hydraulic load, discharge concentrations of Cu are low. With the increase of hydraulic

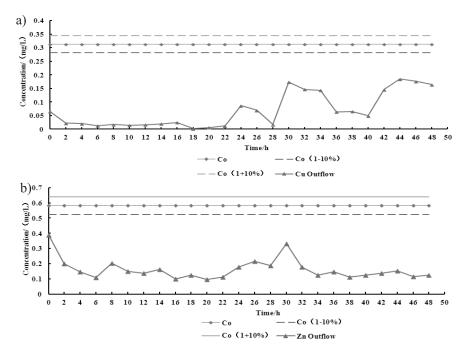


Fig. 8. Exhausted experiment result of No. 10 bioretention tank.

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Test number	Device number	Influent Zn concentration /(mg/L)	Influent water volume /(L)	Rainfall time interval /(d)	Filler factor /(10 ⁻³ d/m)	Zn removal rate /(%)
	7	0.37	529.73	7	552.241	79.7
Test 1	9	0.37	532.14	7	150.218	60.4
	10	0.37	520.69	7	135.264	69.3
	7	0.61	536.49	7	552.241	62.4
Test 2	9	0.61	535.11	7	150.218	59.6
	10	0.61	532.53	7	135.264	70.3
	7	0.53	525.88	15	552.241	87
Test 4	9	0.53	539.16	15	150.218	80.1
	10	0.53	525.43	15	135.264	80.9
	7	0.51	532.82	7	552.241	78.1
Test 5	9	0.51	525.21	7	150.218	73.2
	10	0.51	515.11	7	135.264	78.8
Test 6	7	0.48	546.71	3	552.241	53.6
	9	0.48	533.03	3	150.218	50.4
	10	0.48	524.76	3	135.264	60.3
	7	0.48	353.76	7	552.241	82.3
Test 7	9	0.48	361.49	7	150.218	73.6
	10	0.48	359.63	7	135.264	77.4
	7	1.1	518.86	7	552.241	83.6
Test 9	9	1.1	517.71	7	150.218	73.7
	10	1.1	503.54	7	135.264	70.6

Table 4. Modeling samples of Zn concentration removal rate and its impact factors.

load, discharge concentrations of Cu also show an increasing trend. The discharge concentration of Zn is relatively stable. The purification of bioretention on heavy metals mainly depends on surface layer medium interception and internal medium physical-adsorption; most of the particulate heavy metals are adsorbed on the suspended solids and will be removed through filtering in the surface [13]. Concentrations of particle states of Cu, Zn, Pb, and Cd accounted for 67%, 52%, 97%, and 83%, and Zn has the highest dissolved state proportion [14]. Because the dissolved metals are easily absorbed, with the increase of the influent load, Cu absorbed on soil particle surface will be washed off to increase effluent concentration.

Modeling and Analysis of Zn Removal Effect Based on PLS Method

In the statistical analysis of efficiency of Zn removal, only one dependent variable Y (Zn removal rate) was set with the independent variable X, including water pollutant concentrations, water hydraulic load, rainfall time interval, and filler factor. The drying time and packing factor were found to have a strong linear

relationship with the removal rate of pollutants via curve analysis.

$$\hat{y} = b_0 + b_1 x_1 + b_2 x_2 + b_3 x_3 + b_4 x_4 \tag{3}$$

...where y = Zn removal rate (%), x_1 = influent concentration (mg/L), x_2 = water hydraulic load (L), x_3 = rainfall time interval (d), and x_4 = filler factor (filler adsorption amount divided by the infiltration rate) (10⁻³ d/m).

The Nash-Sutcliffe coefficient of efficiency E is one of the indices most frequently used to assess the accuracy of hydrologic models [19]. It is calculated according to:

$$E = 1 - \frac{\sum_{i=1}^{N} (X_i - Y_i)^2}{\sum_{i=1}^{N} (Y_i - \overline{Y})^2}$$
(4)

...where X_i is the predicted (simulated) value, Y_i is the monitored value, and \overline{Y} is the average of all monitored values. E=1 indicates complete agreement between the measured and calculated values. A negative value of E means that the forecast is not satisfactory. Pearson

Test number	Device number	Influent Zn concentration /(mg/L)	Influent water volume /(L)	Rainfall time interval /(d)	Filler factor /(10 ⁻³ d/m)	Zn removal rate /(%)	Zn predicted values /%
	7	0.58	526.03	7	552.241	79.7	69.98
Test 3	9	0.58	531.52	7	150.218	60.4	58.68
	10	0.58	520.81	7	135.264	69.3	73.58
Test 8	7	0.51	507.05	7	552.241	62.4	73.26
	9	0.51	525.44	7	150.218	51.3	53.69
	10	0.51	534.41	7	135.264	70.3	75.13

Table 5. Test samples of measured and predicted Zn removal rates and impact factors.

correlation coefficient R² measures the linear dependence of measured and calculated values.

Twenty-one groups of data from seven rainfall events were considered as modeling samples. The modeling samples are listed in Tables 4 and 5, and Tests 3 and 8 were used in the model verification. The calibrated original variable model is shown as Eq. (5).

$$\hat{y} = 6.9594 + 0.1776x_1 - 0.3403x_2 + 0.7939x_3 + 0.2503x_4$$
(5)

The simulation results are shown in Fig. 9a). The E values of calibration and validation are, respectively, 0.646 and 0.768. The correlation coefficient R² between all simulated values and measured values is 0.654. These show that the simulated values fit well with measured values.

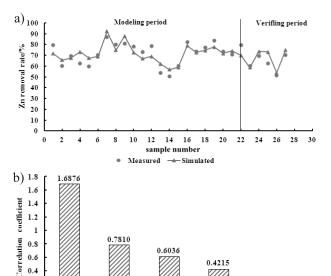


Fig. 9. Modeling of Zn removal effect based on PLS method: a) Comparison of simulated and measured values, b) Importance analysis of influencing factors.

Inflow

Influencing factor

0.4215

Inflow

0.6

0.4

0.2

Rainfall

Filler

Among the four relatively important factors, rainfall time interval, influent concentration, and influent volume are the external influence factors for bioretention, whereas filler factor size is an internal factor. Through correlation calculation (Fig. 9b), rainfall time interval with the correlation coefficient value of 1.6876 is concluded to be the most important factor influencing Zn removal effect; the other important factors are filler characteristic, influent volume, and influent concentration in turn.

Conclusions

As a typical rainwater runoff control measure, bioretention combines the LID technology with rainwater reuse technologies and optimizes the best management practices with the highest use value. Through influence factor experiments, intermittent operation experiments, and continuous operation experiments, as far as the heavy metal removal effects are concerned, fly ash was better than planting soil, and blast furnace slag was the worst; heavy metal removal effect on high influent concentrations was better than on low influent concentrations; the removal efficiency of heavy metals increased with rainfall time interval; and temperature did not affect the removal efficiency of heavy metals on the whole, and effluent heavy metal concentration decreased with time during each test. Rainfall time interval was the most important factor influencing Zn removal effect; the other important factors are filler, influent volume, and influent concentration — in that order.

In future research, the influences of such factors as plant root density, and microbial species and quantity on bioretention purification effects can be explored; the number of influence factor levels should be increased to obtain a better grasp on the characteristics of running parameters about the system; the pollutant migration conversion process in bioretention system should be analyzed and understood; and the purification mechanism model for the bioretention system can be established.

Acknowledgements

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